

Figure 2.2 Concentration of reactant and products for parallel first-order reactions.

# 2.4 SERIES FIRST-ORDER REACTIONS

It is by no means uncommon for a chemical reaction to take place in steps.

$$A \xrightarrow{k_1} B \xrightarrow{k_2} C \tag{2.51}$$

In this case, B is known as an *intermediate* because it is not the final product. A similar situation is very common in nuclear chemistry where a nuclide decays to a daughter, which is also radioactive and undergoes decay. For simplicity, only the case of first-order reactions will be treated here.

The rate of disappearance of A can be written as

$$-\frac{\mathrm{d[A]}}{\mathrm{dt}} = k_1[A] \tag{2.52}$$

The change in concentration of B with time is

$$\frac{d[B]}{dt} = k_1[A] - k_2[B]$$
 (2.53)

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(2.52)

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(2.53)

where the term  $k_1[A]$  represents the formation of B from A, and the term  $-k_2[B]$  represents the reaction of B to form C. The rate of formation of C can be expressed as

$$\frac{\mathrm{d}[\mathrm{C}]}{\mathrm{d}t} = k_2[\mathrm{B}] \tag{2.54}$$

If the stoichiometry as shown in Eq. (2.51) is followed, it is obvious that

$$[A] + [B] + [C] = [A]_0$$
 (2.55)

Eq. (2.52) can be integrated immediately to give

$$[A] = [A]_o \exp(-k_1 t)$$
 (2.56)

Substituting for [A] in Eq. (2.53) gives

$$\frac{d[B]}{dt} = k_1[A]_0 \exp(-k_1 t) - k_2[B]$$
 (2.57)

which can be written as

$$\frac{d[B]}{dt} + k_2[B] - k_1[A]_0 \exp(-k_1 t) = 0$$
 (2.58)

This is a linear differential equation with constant coefficients. If we assume a solution of the form

$$[B] = u \exp(-k_2 t)$$

then

$$\frac{d[B]}{dt} = -uk_2 \exp(-k_2 t) + \exp(-k_2 t) \frac{du}{dt}$$

Substituting the right-hand side of this equation for d[B]/dt in Eq. (2.58), we obtain

$$-uk_{2} \exp(-k_{2}t) + \exp(-k_{2}t) \frac{du}{dt} = k_{1}[A]_{0} \exp(-k_{1}t) - uk_{2} \exp(-k_{2}t)$$

which simplifies to

$$\exp(-k_2 t) \frac{\mathrm{d}u}{\mathrm{d}t} = k_1 [A]_0 \exp(-k_1 t)$$

Dividing both sides of this equation by  $\exp(-k_2t)$  gives

$$\frac{du}{dt} = k_1 [A]_o \exp(-(k_1 - k_2)t)$$
 (2.59)

Figure 2.3

Integration of this equation yields

$$u = \frac{k_1}{k_2 - k_1} [A]_0 \exp(-(k_1 - k_2)t) + C$$
 (2.60)

where C is a constant. Having assumed a solution of the form

$$[B] = u \exp(-k_2 t)$$

we obtain

[B] = 
$$u \exp(-k_2 t) = \frac{k_1 [A]_0}{k_2 - k_1} \exp(-k_1 t) + C \cdot \exp(-k_2 t)$$
 (2.61)

If we let  $[B]_o$  be the concentration of B present at t = 0, Eq. (2.61) reduces to

$$[B]_o = \frac{k_1[A]_o}{k_2 - k_1} + C$$

so that the final equation for the concentration of B is

[B] = 
$$\frac{k_1[A]_0}{k_2 - k_1} (\exp(-k_1 t) - \exp(-k_2 t)) + [B]_0 \exp(-k_2 t)$$
 (2.62)

The first term on the right-hand side of Eq. (2.62) gives the reaction of B produced by disappearance of A, while the second term gives the reaction of any B initially present. If, as is usual,  $[B]_0 = 0$ , Eq. (2.62) reduces to

[B] = 
$$\frac{k_1[A]_o}{k_2 - k_1} (\exp(-k_1 t) - \exp(-k_2 t))$$
 (2.63)

If this result and that shown for [A] in Eq. (2.56) are substituted into Eq. (2.55), we obtain

[C] = [A]<sub>o</sub> 
$$\left[ 1 - \frac{1}{k_2 - k_1} (k_2 \exp(-k_1 t) - k_1 \exp(-k_2 t)) \right]$$
 (2.64)

A number of interesting cases can arise depending on the relative magnitudes of  $k_1$  and  $k_2$ . Figure 2.3 shows the unlikely case where  $k_1 = 2k_2$ . This case is unlikely because the intermediate, B, is usually more reactive than A, as shown in Figure 2.4 where  $k_2 = 2k_1$ . In this case, it is apparent that there is a less rapid decrease in [A] and a slower buildup of B in the system. Because of the particular relationship chosen for the rate constants ( $k_1 = 2k_2$  and  $k_2 = 2k_1$ ), production of C is unchanged in the two cases. Figure 2.5 shows the case where  $k_2 = 10k_1$  as

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$$xp(-k_2t)$$
 (2.61)

Eq. (2.61) reduces to

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$$(-k_2^{\dagger}t)$$
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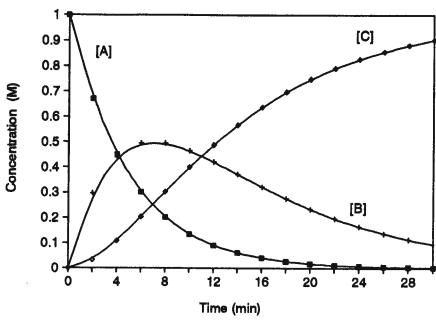
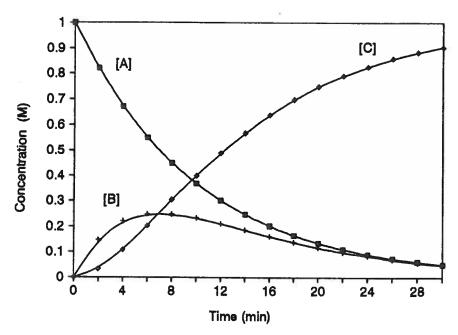
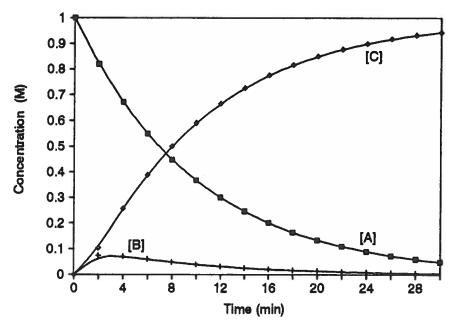


Figure 2.3 Series first-order reactions where  $[A]_0 = 1.00 \text{ M}$ ,  $k_1 = 0.200 \text{ and } k_2 = 0.100 \text{ min}^{-1}$ .



**Figure 2.4** Series first-order reactions where  $[A]_0 = 1.00 \text{ M}$ ,  $k_1 = 0.100 \text{ and } k_2 = 0.200 \text{ min}^{-1}$ .



**Figure 2.5** Series first-order reactions where  $[A]_0 = 1.00 \text{ M}$ ,  $k_1 = 0.100 \text{ and } k_2 = 1.00 \text{ min}^{-1}$ .

a realistic example of a system with a reactive intermediate. In this case, the concentration of B is always low, which is more likely for an intermediate. Further, over a large extent of reaction, [B] is essentially a constant. When  $k_2 > k_1$ , there is a low and essentially constant concentration of intermediate, B. Therefore, d[B]/dt is essentially 0, which can be shown as follows. For this system of first-order reactions,

$$[A] + [B] + [C] = [A]_{o}$$

which, because [B] is nearly 0, is approximated by

$$[A] + [C] = [A]_0$$

Taking the derivatives with respect to time,

$$\frac{d[A]}{dt} + \frac{d[B]}{dt} + \frac{d[C]}{dt} = 0$$

and

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$$\frac{d[A]}{dt} + \frac{d[C]}{dt} = 0$$

 $M_1$ ,  $k_1 = 0.100$  and  $k_2 = 1.00$  min<sup>-1</sup>.

nediate. In this case, the conor an intermediate. Further, astant. When  $k_2 > k_1$ , there is intermediate, B. Therefore, ws. For this system of firstTherefore d[B]/dt = 0, and [B] remains constant throughout most of the reaction. For the case where  $k_2 = 10k_1$  and  $[A]_0 = 1.00$  M (shown in Figure 2.5), [B]never goes above 0.076 M and it varies only from 0.076 to 0.033 M from t = 2min to t = 12 min where [A] varies from 0.819 to 0.301 M and [C] varies from 0.105 M to 0.666 M. The approximation of considering the concentration of the intermediate to be essentially constant is called the *steady-state approximation*.

It is clear from Figures 2.3 through 2.5 that [B] goes through a maximum as expected. The time necessary to reach that maximum concentration of B, t,, can easily be calculated. At that time, d[B]/dt = 0. If Eq. (2.63) is differentiated with respect to time,

$$\frac{d[B]}{dt} = \frac{-k_1 k_1 [A]_o}{k_2 - k_1} \exp(-k_1 t) + \frac{k_1 k_2 [A]_o}{k_2 - k_1} \exp(-k_2 t) = 0$$
 (2.65)

Therefore,

$$\frac{k_1 k_1 [A]_o}{k_2 - k_1} \exp(-k_1 t) = \frac{k_1 k_2 [A]_o}{k_2 - k_1} \exp(-k_2 t)$$

Cancelling like terms from both sides of the equation gives

$$k_1 \exp(-k_1 t) = k_2 \exp(-k_2 t)$$

which can be written as

$$k_1/k_2 = \exp(-k_2t)/\exp(-k_1t) = \exp(-k_2t)(\exp(k_1t)) = \exp((k_1 - k_2)t)$$

Taking the logarithm of both sides of the equation gives

$$\ln(k_1/k_2) = (k_1 - k_2)t$$

which yields the time to reach the maximum in the [B] curve,

$$t_{m} = \frac{\ln(k_{1}/k_{2})}{k_{1} - k_{2}}$$
 (2.66)

Although several other cases of series of reactions have been described mathematically, we will leave these discussions to more advanced books. The basic principles have been adequately demonstrated here.

### 2.5 **REVERSIBLE REACTIONS**

Many reactions do not proceed to completion, and the extent of reversibility must be considered from the early stages. The first-order case is the simplest.

# Principles of Chemical Kinetics

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